



First Order Derivatives of Thermodynamic Functions under Assumption of no Chemical Changes



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DIFFERENTIALS

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The total differential of a function f of several variables is the sum of all partial differentials [1]. In the absence of chemical changes, all state thermodynamic parameters are total differentials and depend on two variables (Table 1).

Table 1. Differentials of thermodynamic parameters

$dE = T \cdot dS - p \cdot dV + \sum_i \mu_i \cdot dn_i$	in the presence of chemical changes
$dn_i = 0$ for each i	provided that no chemical changes
$dE = T \cdot dS - p \cdot dV$	in the absence of chemical changes
E = internal energy; S = entropy; V = volume; n = number of particles	

[1] M. Hazewinkel, Encyclopaedia of Mathematics: An Updated and Annotated Translation of the Soviet "Mathematical Encyclopaedia." Dordrecht, Netherlands: Reidel, 1988, p. 228.

OBJECTIVES

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- Identifying the heat from reversible process $dQ_{\text{rev}} = T \cdot dS$ and mechanical work in the form of that from quasi-static processes $dw_{\text{cvs}} = -p \cdot dV$, these two thermodynamic quantities (dQ and dw) became total differentials. The condensed collection of the Bridgman's thermodynamic equations [2] was used as starting point in this study. A series of codification schemas were developed and implemented in order to obtain all first order partial derivatives [3] (Table 2).

[2] P.W. Bridgman, A complete collection of thermodynamic formulas, Phys. Rev. 3, 1914, 273-281.

[3] L. Jäntschi, General Chemistry Course, AcademicDirect Publishing House, 2013.

BRIDGMAN'S THERMODYNAMIC EQUATIONS

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Table 2. Gradients after pressure (p), volume (V) and temperature (T) of an unknown function (f)

Variable			$\left. \frac{\partial f}{\partial x} \right _{z=ct} = \left. \frac{\partial f}{\partial x} \right _{y=ct} + \left. \frac{\partial f}{\partial y} \right _{x=ct} \cdot \left. \frac{\partial y}{\partial x} \right _{z=ct}$	$\left. \frac{\partial f}{\partial z} \right _{x=ct} = \left. \frac{\partial f}{\partial y} \right _{x=ct} \cdot \left. \frac{\partial y}{\partial z} \right _{x=ct}$	Order
z	x	y	$f_{xz} = f_{xy} + f_{yx} \cdot y_{xz}$	$f_{zx} = f_{yx} \cdot y_{zx}$	$f = E$
p	T	V	$f_{pV} = f_{pT} + f_{Tp} \cdot T_{pV}$	$f_{Vp} = f_{Tp} \cdot T_{Vp}$	6
p	V	T	$f_{pT} = f_{pV} + f_{Vp} \cdot V_{pT}$	$f_{Tp} = f_{Vp} \cdot V_{Tp}$	5
T	p	V	$f_{TV} = f_{Tp} + f_{pT} \cdot p_{TV}$	$f_{VT} = f_{pT} \cdot p_{VT}$	2
T	V	p	$f_{Tp} = f_{TV} + f_{VT} \cdot V_{Tp}$	$f_{pT} = f_{VT} \cdot V_{pT}$	4
V	p	T	$f_{VT} = f_{Vp} + f_{pV} \cdot p_{VT}$	$f_{TV} = f_{pV} \cdot p_{TV}$	1
V	T	p	$f_{Vp} = f_{VT} + f_{TV} \cdot T_{Vp}$	$f_{pV} = f_{TV} \cdot T_{pV}$	3

RESULTS

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- Inputs: state parameters, process differentials, thermodynamic equations and gradients.
- Output: first order partial derivatives, counting a number of two-hundred and forty equations
- <http://l.academicdirect.org/Chemistry/ChemPhys/>

RESULTS

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Typesetting math: 26%

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Equations: 240

RESULTS

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State parameters			Process differentials		
Type	Parameter	Meaning	Type	Parameter	Meaning
Intensive	P	Pressure	Extensive	dQ	Heat
Intensive	T	Temperature	Extensive	dw	Work
Extensive	V	Volume	Extensive	$dQ_r \stackrel{\text{def}}{=} T \cdot dS$	Reversible heat
Extensive	S	Entropy	Extensive	$dw_c \stackrel{\text{def}}{=} -p \cdot dV$	Quasistatic work
Extensive	E	Internal energy	Consequence		
Extensive	N	Number of particles	A reversible process is quasistatic		
Extensive	$H \stackrel{\text{def}}{=} E + pV$	Enthalpy	Equations		
Extensive	$A \stackrel{\text{def}}{=} E - TS$	Helmholtz energy	Equation	Comments	
Extensive	$G \stackrel{\text{def}}{=} E + pV - TS$	Gibbs energy	$dE = dQ + dw$	for a system with no chemical changes	
Exact	N_A	Avogadro's number of particles	$dE = dQ + dw + \sum_i \mu_{N,i} dN_i$	general law ($\mu_i \stackrel{\text{def}}{=} N_A \mu_{N,i}$)	
Extensive	$n \stackrel{\text{def}}{=} \frac{N}{N_A}$	Amount of substance (mols)	$dE = dQ + dw + \sum_i \mu_i dn_i$		
Intensive	$V_m \stackrel{\text{def}}{=} \frac{V}{n}$	Molar volume	$E = Q + w + \sum_i \int \mu_i dn_i$	Integral general law (assumes null integration constant)	
Intensive	$S_m \stackrel{\text{def}}{=} \frac{S}{n}$	Molar entropy	$dE = dQ - pdV + \sum_i \mu_i dn_i$	quasistatic ($dw = -pdV$) processess	
Intensive	$E_m \stackrel{\text{def}}{=} \frac{E}{n}$	Molar internal energy	$dH = dQ + Vdp + \sum_i \mu_i dn_i$		
Intensive	$H_m \stackrel{\text{def}}{=} \frac{H}{n}$	Molar enthalpy	$dA = dQ - pdV - TdS - SdT + \sum_i \mu_i dn_i$		
Intensive	$A_m \stackrel{\text{def}}{=} \frac{A}{n}$	Molar Helmholtz energy	$dG = dQ + Vdp - TdS - SdT + \sum_i \mu_i dn_i$	reversible ($dQ = TdS$) & quasistatic ($dw = -pdV$) processess	
Intensive	$G_m \stackrel{\text{def}}{=} \frac{G}{n}$	Molar Gibbs energy	$dE = TdS - pdV + \sum_i \mu_i dn_i$		
Intensive	$J \stackrel{\text{def}}{=} \frac{2E}{pV}$	Number of energy components	$dH = TdS + Vdp + \sum_i \mu_i dn_i$		
			$dA = -pdV - SdT + \sum_i \mu_i dn_i$		
			$dG = Vdp - SdT + \sum_i \mu_i dn_i$		

RESULTS

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Gradients

Gradient	Formula
Isothermal compresibility	$\beta_T \stackrel{\text{def}}{=} -\frac{1}{V} \cdot \frac{\partial V}{\partial p} \Big _{T=\text{ct.}}$
Volumetric coefficient of thermal expansion	$\alpha_V \stackrel{\text{def}}{=} \frac{1}{V} \cdot \frac{\partial V}{\partial T} \Big _{p=\text{ct.}}$
Heat capacity at constant pressure	$C_p \stackrel{\text{def}}{=} \frac{\partial H}{\partial T} \Big _{p=\text{ct.}}$
Joule-Thomson isothermal coefficient	$\mu_T \stackrel{\text{def}}{=} \frac{\partial H}{\partial p} \Big _{T=\text{ct.}}$
Heat capacity at constant volume	$C_V \stackrel{\text{def}}{=} \frac{\partial E}{\partial T} \Big _{V=\text{ct.}}$
Internal pressure	$\pi_T \stackrel{\text{def}}{=} \frac{\partial E}{\partial V} \Big _{T=\text{ct.}}$

To do: first and second partial derivatives

$$\frac{\partial E}{\partial G} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{S \cdot V + S \cdot p \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} + p \cdot V \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

$$\frac{\partial E}{\partial H} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{S \cdot V + p \cdot V \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - p \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}}}$$

$$\frac{\partial E}{\partial Q} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

$$\frac{\partial E}{\partial S} \Big|_{A=\text{ct.}} = \frac{-p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}} - p \cdot T \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}{-\frac{p \cdot \frac{\partial H}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial p} \Big|_{T=\text{ct.}}}{T} - \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}} - S \cdot \frac{\partial V}{\partial T} \Big|_{p=\text{ct.}}}$$

FUTHER WORK

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- The transformation of an interactive interrogation is conducted in our lab in order to allow selecting the function, the variable and the constant before generation of the thermodynamic equation first order derivatives.

Thank you for your attention!

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